

Partie 2:

1) Equilibre d'un élément de vapeur

$$[-P(z+dz) + P(z)] \mu (\delta-y) + \rho_L g \mu (\delta-y) dz - \mu_L \frac{du}{dy} dz \mu = 0$$

$$\Rightarrow \left[-\frac{dP}{dz} + \rho_L g \right] (\delta-y) = \mu_L \frac{du}{dy}$$

Dans la vapeur $\frac{dP}{dz} = \rho_v g$

$$\Rightarrow \mu_L \frac{du}{dy} = (\rho_L - \rho_v) g (\delta-y)$$

2) Conditions aux limites $\frac{du}{dy} = 0$ en $y = \delta$ et $u = 0$ en $y = 0$

d'où $u(y) = \frac{(\rho_L - \rho_v) g}{\mu_L} \left(\delta y - \frac{y^2}{2} \right)$

$$3) m(z) = \rho_L L \int_0^\delta u(y, z) dy = \rho_L L \frac{(\rho_L - \rho_v) g}{\mu_L} \left[\delta \frac{y^2}{2} - \frac{y^3}{6} \right]_0^\delta = \frac{\rho_L (\rho_L - \rho_v) g}{\mu_L} L \frac{\delta^3}{3}$$

4) Bilan thermique

$dq = k_L \frac{dT}{dy}$ densité de flux. Puissance $dW = k_L \frac{dT}{dy} L dy$

$$5) dW = k_L \frac{(T_{sat} - T_c)}{\delta} L dy = h_{LV} dm = h_{LV} \frac{\rho_L (\rho_L - \rho_v) g}{\mu_L} L \delta^2 \frac{d\delta}{dz}$$

$$\Rightarrow \delta = \left[\frac{4 \mu_L k_L (T_{sat} - T_c)}{\rho_L (\rho_L - \rho_v) g h_{LV}} z \right]^{1/4}$$

$$6) dm = \frac{k_L (T_{sat} - T_c) L}{h_{LV}} dz \times \left[\frac{\rho_L (\rho_L - \rho_v) g h_{LV}}{4 \mu_L k_L (T_{sat} - T_c)} z \right]^{1/4}$$

$$m(z) = \left[\frac{k_L (T_{sat} - T_c)}{h_{LV}} \right]^{3/4} L \left[\frac{\rho_L (\rho_L - \rho_v) g}{4 \mu_L} \right]^{1/4} z^{3/4} \times \frac{4}{3}$$

$$m(z) = \left[\frac{4 k_L (T_{sat} - T_c)}{h_{LV}} \right]^{3/4} \left[\frac{\rho_L (\rho_L - \rho_v) g}{\mu_L} \right]^{1/4} \frac{L}{3} z^{3/4}$$

$$\dot{m} = \left[\frac{4 k_L (T_{sat} - T_c)}{h_{LV}} \right]^{3/4} \left[\frac{\rho_L (\rho_L - \rho_v) g}{\mu_L} \right]^{1/4} \frac{L \times 4}{21} \dot{z}^{7/4}$$

La puissance à évacuer $W = 300 \text{ W}$

$$W = 2 h_{LV} \dot{m} \Rightarrow h = 4 \text{ mm}$$