

1) Liquid and wall temperature

$$G \pi \frac{D^2}{4} C_p \frac{dT}{dz} = q_p \pi D \rightarrow T_L(z) = T_{Le} + \frac{4q_p z}{D G C_p}$$

$$q_p = h_L (T_p - T_L(z)) \rightarrow T_p = T_L(z) + \frac{q_p}{h_L}$$

with  $h_L = 570 \text{ W/m}^2/\text{K}$

$$2) z_{\text{sat}} = \frac{(T_{\text{sat}} - T_{Le}) D G C_p}{4q} = 0.281 \text{ m}$$

$$T_p = 56.92^\circ\text{C}$$

$$T_p - T_{\text{sat}} = 17.52 > \left[ \frac{8 \sigma T_{\text{sat}} q}{\lambda \rho_v h_{lv}} \right]^{1/2} \frac{1}{fr} = 0.153$$

The wall temperature is larger than the temperature for the onset of nucleate boiling

$$3) \text{ For } z > z_{\text{sat}} \quad G \pi \frac{D^2}{4} h_{lv} \frac{dx}{dz} = q_p \pi D$$

$$x = \frac{4q_p}{D G h_{lv}} (z - z_{\text{sat}})$$

$$z = 0.3 \text{ m} \quad x = 0.0058 \quad \dot{v}_v = \frac{G x}{\rho_v} = 0.023 \text{ m/s}$$

$$\dot{v}_L = 0.172 \text{ m/s} \rightarrow \text{slug flow}$$

$$z = 0.6 \text{ m} \quad x = 0.0977$$

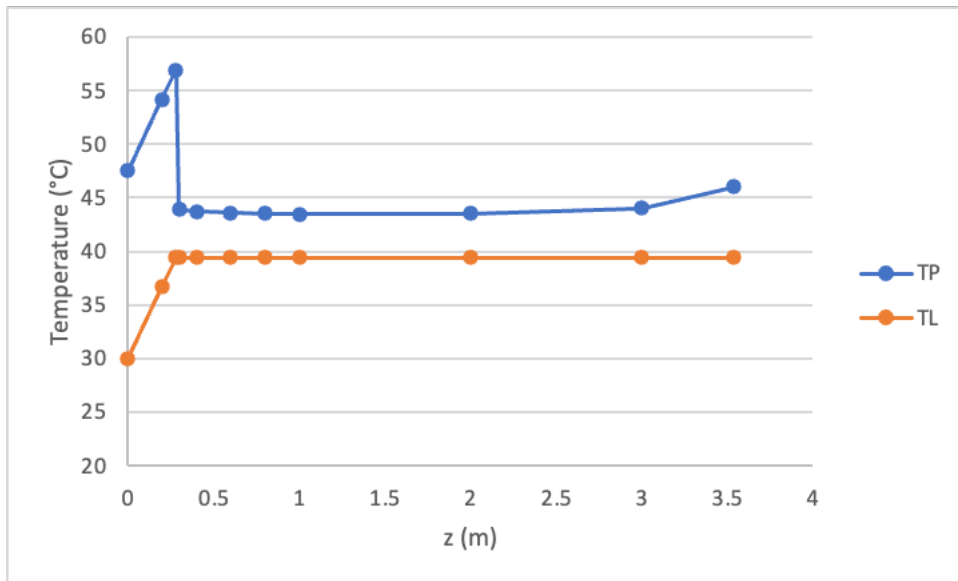
$$\dot{v}_v = 0.392 \text{ m/s} \\ \dot{v}_L = 0.152 \text{ m/s} \left. \vphantom{\begin{matrix} \dot{v}_v \\ \dot{v}_L \end{matrix}} \right\} \text{churn flow}$$

$$\text{Pure vapor } x = 1 \quad z = 3.55 \text{ m}$$

$$4) T_p = T_{\text{sat}} + \frac{q}{h}, \quad h \text{ calculated with Gungor \& Winterton correlation}$$

$$z = 0.3 \text{ m} \quad T_p = 43.9^\circ\text{C}$$

$$z = 0.6 \text{ m} \quad T_p = 43.59^\circ\text{C}$$



5) Void fraction evaluate from the drift flux model

$$U_v = \frac{j_v}{R_G} = C_0 (j_v + j_L) + U_{ao}$$

$$C_0 = 1.2 \quad U_{ao} = 0.35 \sqrt{gD}$$

$$z = 0.3 \text{ m} \quad R_G = 0.076$$

$$z = 0.6 \text{ m} \quad R_G = 0.538$$

$$6) \underbrace{\frac{d}{dz} \left[ \frac{G^2 x^2}{\rho_v R_v} + \frac{G^2 (1-x)^2}{\rho_L (1-R_v)} \right]}_{\text{inertia term}} = \underbrace{-\frac{dP}{dz}}_{\text{pressure gradient}} + \underbrace{\frac{4\bar{G}P}{D}}_{\text{wall friction}} - \underbrace{(\rho_L (1-R_G) + \rho_v R_G)g}_{\text{hydrostatic pressure gradient}}$$

single-phase flow  $z < z_{sat}$

$$-\frac{dP}{dz} + \frac{4\bar{G}P}{D} - \rho_L g = 0 \quad P(z_{sat}) - P(0) = \int_0^{z_{sat}} \left( \frac{2}{D} \bar{G}P - \rho_L g \right) dz$$

Two-phase flow

$$P(z) - P(z_{sat}) = \frac{4\bar{G}P}{D} (z - z_{sat}) - \rho_L (1 - R_G) g (z - z_{sat}) - \left[ \frac{G^2 x^2}{\rho_v R_v} + \frac{G^2 (1-x)^2}{\rho_L (1-R_v)} - \frac{G^2}{\rho_L} \right]$$